

Amendments to Specification

Please replace the paragraph beginning on page 4, line 14, with the following amended paragraph:

For the purposes of the present invention, "highly fluorinated" means that 50% or greater of the atoms bonded to carbon are fluorine excluding linking atoms such as O or S. Preferred highly fluorinated monomers useful for this invention include fluoroolefins such as those having 2-10 carbon atoms. Preferred monomers also include fluorinated vinyl ethers such as those having the formula $CY_2 = CYOR$ or $CY_2 = CYOR'OR$ wherein Y is H or F, and -R and -R' are independently completely-fluorinated or partially-fluorinated alkyl or alkylene groups containing 1-8 carbon atoms and are preferably perfluorinated. Preferred -R groups contain 1-4 carbon atoms and are preferably perfluorinated. Preferred -R' groups contain 2-4 carbon atoms and are preferably perfluorinated. The most preferred fluorinated monomers for use in the present invention include trifluoroethylene, hexafluoropropylene (HFP), ~~monochlorotrifluoroethylene~~ chlorotrifluoroethylene (CTFE), perfluorobutyl ethylene (PFBE), and perfluoro(alkyl vinyl ether) (PAVE), especially perfluoro(ethyl vinyl ether)(PEVE) and perfluoro(methyl vinyl ether)(PMVE).

Please replace the paragraph beginning on page 14, line 7, with the following amended paragraph:

This comparative example illustrates the polymerization of TFE copolymer with a small amount of PEVE resulting in a polymer with a high melting point. A stirred jacketed stainless steel horizontal autoclave of 11.4 L (3 U.S. gal) capacity is used as the polymerization vessel with a two blade cage-type agitator run at 65 rpm. The autoclave is equipped with instrumentation to measure temperature and pressure and with a compressor that could feed monomer to the autoclave at the desired pressure. The autoclave is filled 6.2 L of deionized water containing 12 g of ammonium perfluorooctanoate (3M Co., St. Paul, MN). The autoclave is then pressured to 2.8 MPa (400 psig) with nitrogen and vented three times followed by similar pressuring and venting with TFE. The autoclave contents are heated to 90°C and 406.6 g TFE and 306.8 g

~~perfluoro(ethyl vinyl ether)~~perfluoro(ethyl vinyl ether) (PEVE) are added to bring the vessel to its working pressure of 2.8 M Pa (400 psig). Initiator solution is prepared by dissolving 5 g ammonium persulfate in 1 L of deionized water. The initiator solution is fed to the reactor at a rate of 25 mL/min for a period of five minutes, then the rate is reduced and maintained at 1 mL/min for the duration of the experiment. The autoclave is operated in a semibatch fashion in which a monomer mixture in weight ratio 85/15 TFE/PEVE is added to the reactor to maintain constant pressure as polymerization occurred. A total of 1700.8 g TFE and 300.0 g PEVE is added during the run. After about 1-1/2 hrs. the feed is stopped, the contents of the autoclave are cooled, and excess monomers are vented. The polymer dispersion is discharged to a receiver as a turbid homogeneous mixture containing 23.1 wt. % solid. Polymer is isolated freezing the dispersion then collecting the product on a suction filter. The filter cake is washed with water and dried in a convection oven at 90-100°C to yield 1973 g copolymer containing 88.0 wt% TFE and 12 wt % PEVE. The DSC of the polymer displays a melting endotherm with a peak temperature of 277°C. Melt viscosity as determined at 372°C is 410 Pa•sec.